



TECHNOLOGY-SPECIFIC LIFE CYCLE ASSESSMENT CONTRIBUTING TO AN ENERGY STRATEGY

51th LCA Discussion Forum
THE ROLE OF ENVIRONMENTAL LIFE CYCLE THINKING IN
LONG-TERM (ENERGY) STRATEGIES



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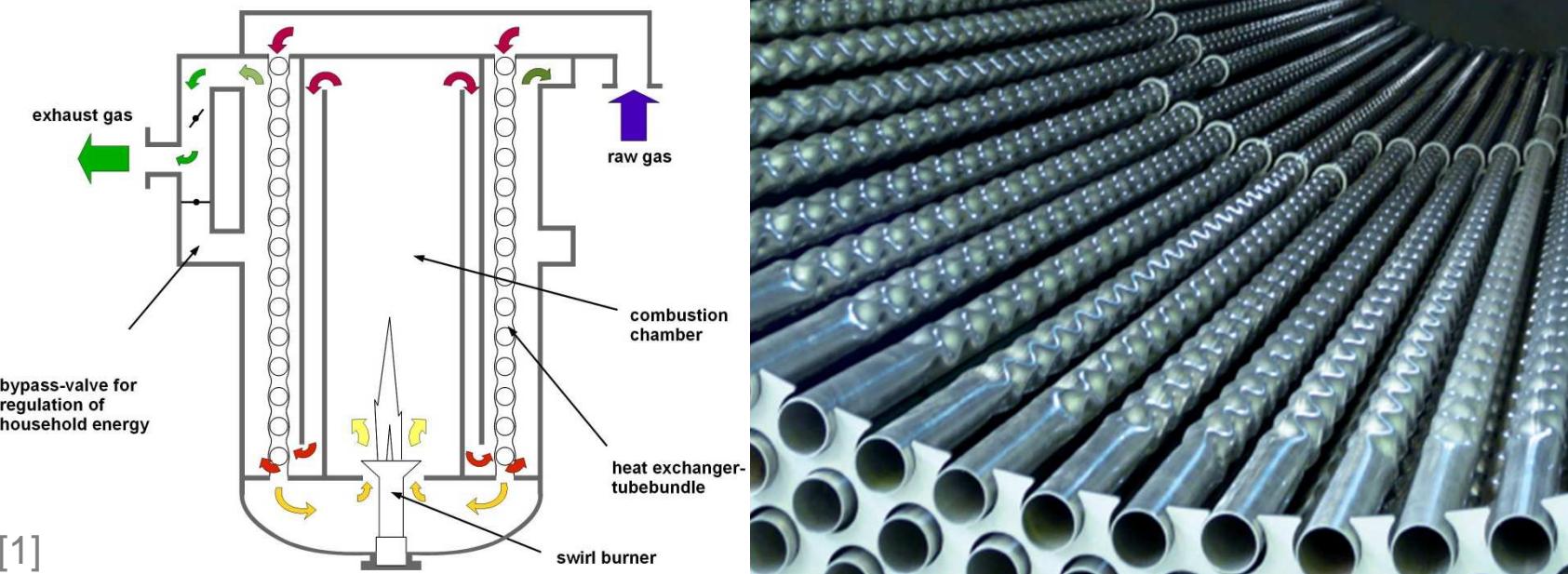
Bern 25. 04. 2013

AGENDA

1. Technological Development
2. Fire Tube Boiler
3. Functional Unit
4. Bottom up-Top down-Approach
5. Inventarisation
6. Impact Assessment
7. Evaluation
8. Discussion and Outlook
9. References

1. Technological Development

2013	LCA of an improved fire tube boiler	HTW Berlin
2013-2016	Micro-profiled Plate Heat Exchanger	TTZ GmbH
2009-2012	Thermochemical Storage Unit	TH Wildau
2009-2011	Integrated Algae Reactor System	TH Wildau
2008-2011	High-end Product Gas Cooler	TU Berlin/UNott
2006-2008	High-performance Forming Machine	Omega/Contec

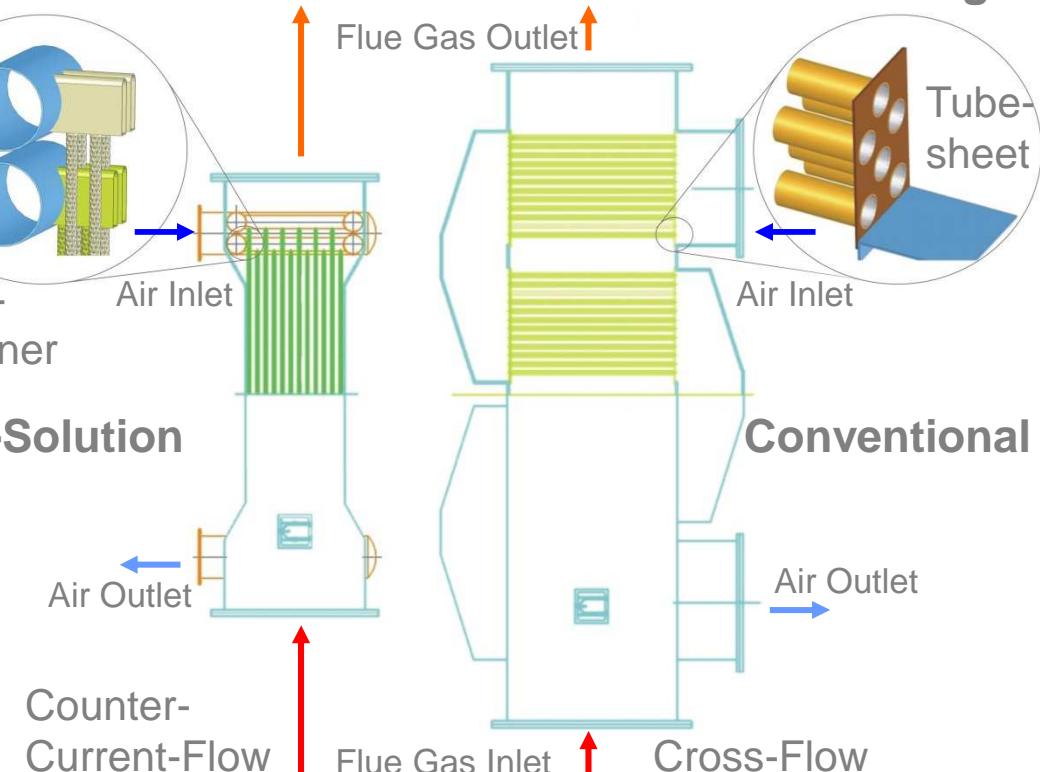


Construction Methodology: Concept Functionalisation of Assembly Units



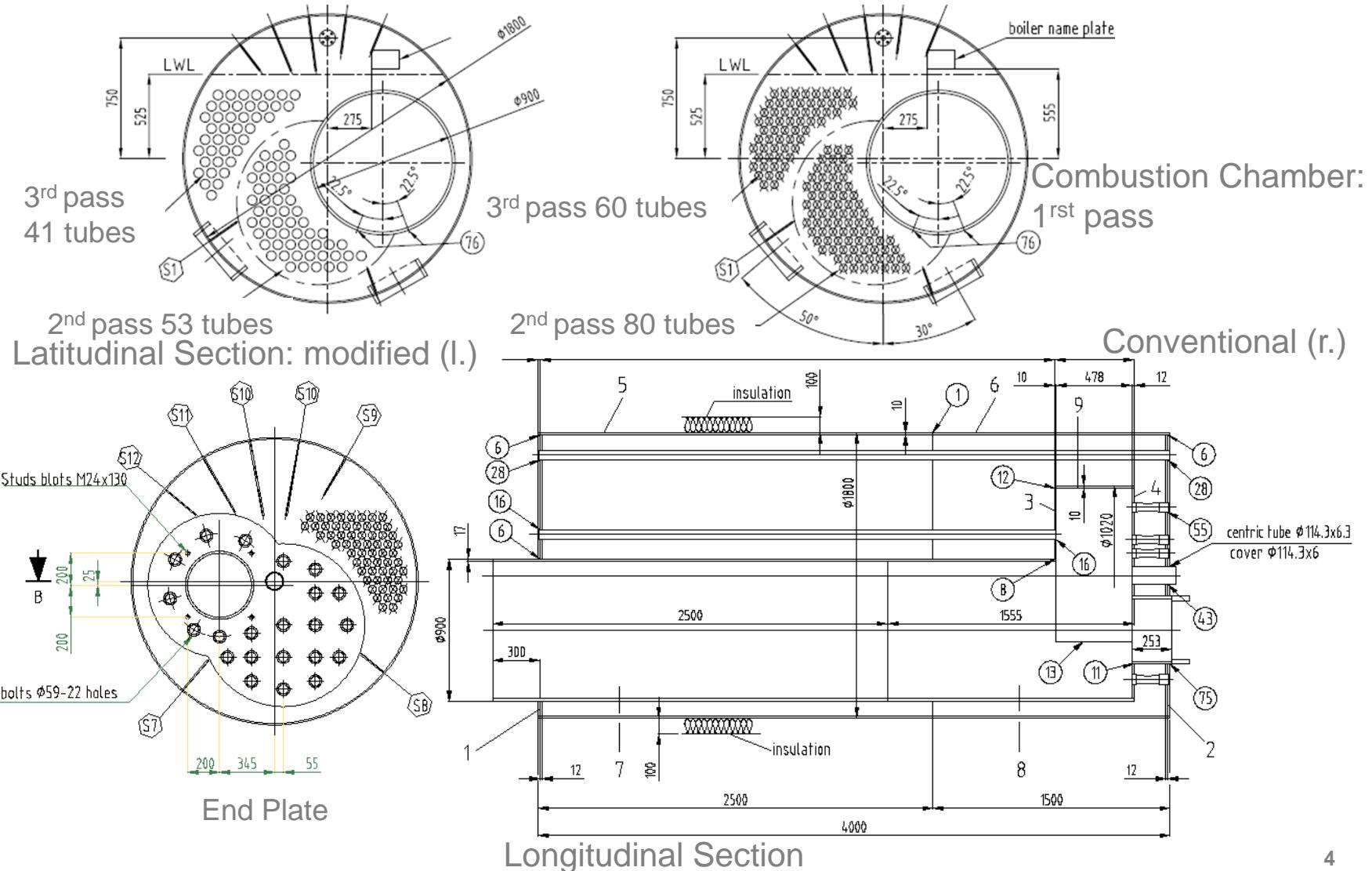
Functional Elements
↓
**Specific Surface
Structure Technology**

Assembly Surfaces → Active Functional Elements
FAU-Concept → Functionalisation +
New Constructional Design





2. Fire Tube Boiler



3. Functional Unit

Specific Data			Variants
Quantity	Value	Unit	
Steam Mass Flow	3500	$\text{kg s} \cdot \text{h}^{-1}$	Process Steam
Steam Pressure	11	bar	Process Heat
Steam Temperature	184	°C	Electricity 350 kW *
Natural Gas LL*	33.400	$\text{MJ} \cdot \text{m}^{-3}$	* $\eta_G = 15\%$, Steam Turbine- (Siemens AG Görlitz)
Gas Flow (3 bar g)	260	$\text{m}_N^3 \cdot \text{h}^{-1}$	Steam Motor- Gen Set-Condenser
Air Flow	2573	$\text{m}_N^3 \cdot \text{h}^{-1}$	(Spilling Energie Systeme GmbH Hamburg)
Flue Gas Flow	2835	$\text{m}_N^3 \cdot \text{h}^{-1}$	
Feed Water Flow (105°C)	3600	$\text{kg} \cdot \text{h}^{-1}$	
Thermal Capacity	2281	kW	
Thermal Efficiency	0.9465	-	
Lifetime*	15	a	
Boiler Mass (Tube)*	3288.24	kg	

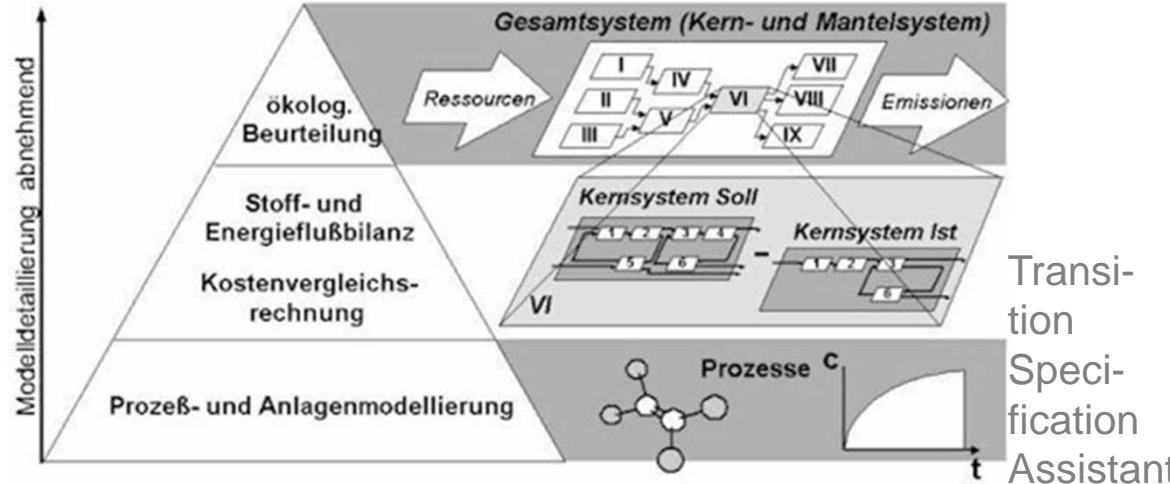
* Shortfall Fuel Mazut (HFO), 30 a/45 a, 1-3 major + 6-18 small revisions
+ Shell, Eco, $\Delta m = 756.24 \text{ kg}$ (-23%), $m_i = 2532$, $\Delta \eta = 1.65\%$, $\eta_0 = 93\%$.



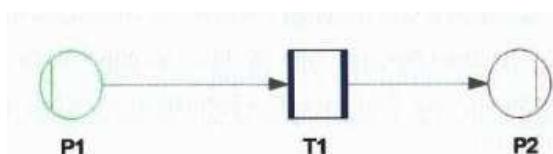
Specific Data corresponding to The Functional Unit 3.5 t_S/h (11 bar, 184 °C)

[4,5] 5

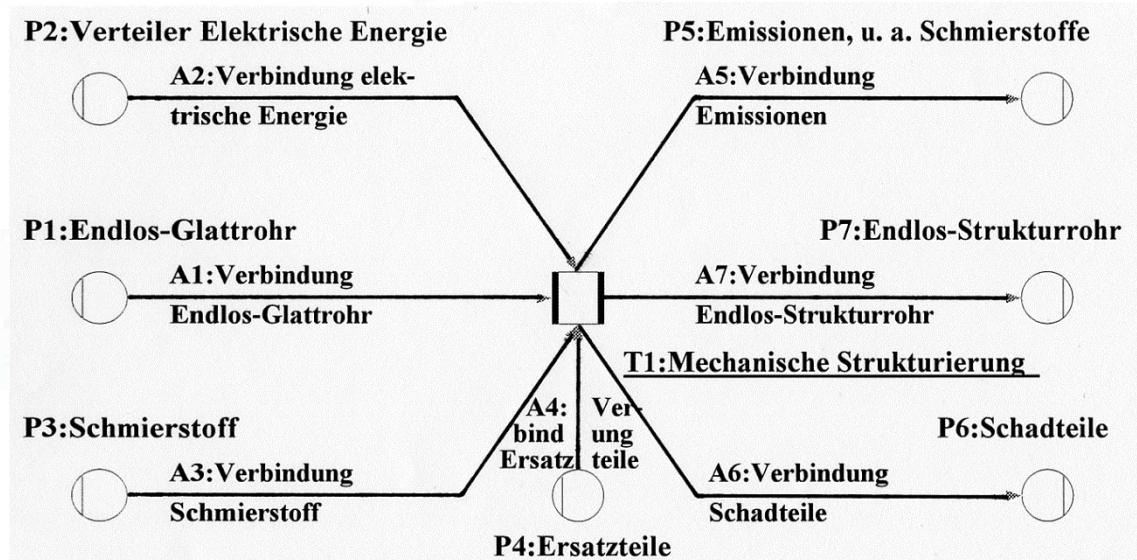
4. Bottom up-Top down-Approach



Core-System Bottom up
Shell-System Top down



Boiler under Construction



[6,7,8]

Specific module of the forming process generated under UMBERTO 6



5. Inventarisation

	CH_4	C_2H_6	$\text{i-C}_4\text{H}_{10}$	$\text{N-C}_5\text{H}_{12}$	C_6H_{14}	N_2	CO_2
	Mol-%						
	81.6	3.1	0.4	0.002	0.001	1.9	13

Gas	Compound	Vol.-%
Nitrogen	N_2	78.08
Oxygen	O_2	20.95
*Water	H_2O	< 4
Argon	Ar	0.93
*Carbon Dioxide	CO_2	0.036
Neon	Ne	0.0018
Helium	He	0.0005
*Methane	CH_4	0.00017
Hydrogen	H_2	0.00005
*Nitrous Oxide	N_2O	0.00003
*Ozone	O_3	0.000004
earthnear, * variable		

Natural Gas LL

$$\Phi_{\Lambda,\text{spec.}} = \sum_{j,o,\pi}^{j,o,\pi} K_{j,o} + \left(\frac{K_\pi}{\Delta t} \right)_m \cdot \int_0^{n_a-1} K_\pi(t) \cdot \left(\frac{1+I(t)}{1+Z(t)-I(t)} \right)^t dt$$

$$\Phi_{X,\text{spec.}} = \sum_1^{i,j,l,m} \Theta_{i,j,l,m}$$

i – Item of the balance
 j – Life Cycle Phase
 l – Type of Term
 m – Number of Term
 o – Type of Cost
 π – Cost Value

Mass-, Energy and Cost Balance

Flue Gas	Vol.-%
CO_2	8.71
H_2O	18.27
N_2	71.32
O_2	1.7

Combustion Air

Flue Gas [9,10] 8

6. Impact Assessment

$$\Phi_{K,spec.} = \sum_{i,j} m_i \cdot f_{\Phi K,i} \cdot f_{AK,i} \cdot P_{j,spec.} \quad \text{Environmental Impact Potential}$$

- m_i = Mass Freight of a Substance,
- $f_{\Phi K,i}$ = Specific Characterisation Factor of the Category K ,
- $f_{AK,i}$ = Specific Allocation Factor of the Category K ,
- $P_{j,spec.}$ = Specific Mass and Energy Turnover of Process Chains,
- i = Index of Substances of the Category K ,
- j = Index of Life Cycle Phases of the Object.

Federal Environmental Agency Potential Method

**Mid Point-orientated Potential:
neither Inventory
nor Damage**

$$\Phi_{K,N,spec.} = \frac{\Phi_{K,spec.}}{\Phi_{K,all}}$$

Normalisation to Reference Frame

$$\Phi_{GW,100,CO_2,i} = \frac{\int_0^{T_H} a_i(t) \cdot \lambda_i(t) dt}{\int_0^{T_H} a_{Ref.}(t) \cdot \lambda_{Ref.}(t) dt}$$

- a = Radiation Impact, $[a] = W \cdot m^{-2} \cdot kg^{-1}$,
- λ = Decay Constant,
- t = Time Coordinate,
- T_H = Time Horizon.

Example: Model of Global Warming Potential 9

7. Evaluation

$$l_K = \frac{\Phi_{K,\text{all}} - \Phi_{K,G}}{\Phi_{K,G}}$$

l_K = Grade of Goal Getting
 $\Phi_{K,\text{all}}$ = Actual Value
 $\Phi_{K,G}$ = Goal Value

$$G_K = \frac{l_K}{\sum_K l_K} \quad \longrightarrow \quad \Xi_{K,i} = G_K \cdot \Phi_{K,N,\text{spec.}}$$

Weighting Coefficient

Objective Goals in Germany until 2020:

- Increased Energy Efficiency by 20 %
- Increased Resource Efficiency by 37.5 %
- Decreased Global Warming Potential by 40 %

$\Delta\eta/\eta_0$	= 1.8 %
$\Phi_{E,N,\text{spec.}}$	= $9.7 \cdot 10^{-8}$
$\Delta m/m_0$	= 0.76 %
$\Phi_{R,N,\text{spec.}}$	= $1.3 \cdot 10^{-9}$
$\Delta V/V_0$	= 0.16 %
$\Phi_{GWP,N,\text{spec.}}$	= $6.4 \cdot 10^{-8}$
G_E	= 0.15
G_R	= 0.37
G_{GWP}	= 0.48

$$\Xi_{K,i} = \Xi_{E,i} + \Xi_{R,i} + \Xi_{GWP,i} = 1.5 \cdot 10^{-8} + 5 \cdot 10^{-10} + 3.1 \cdot 10^{-8} = 4.6 \cdot 10^{-8}$$

Improved Boiler contributes 33% Energy Efficiency and 67 % GWP to Objective Goal

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8. Discussion and Outlook

▪ Best Available Technology

- Successful Re-design of the Boiler and Use of ip tube® Bundles
- Increased Efficiency $\Delta\eta/\eta_0 = 1.8 \%$
- Decreased Boiler Fuel Demand and CO₂-Emission $\Delta V/V_0 = 0.16 \%$
- Decreased Boiler Mass $\Delta m/m_0 = 0.76 \%$

▪ Life Cycle Assessment

- Federal Environmental Agency Potential Method
- Mid Point-Orientation and Normalisation to Reference Frame
- Integration of Objective Goals by Grade of Goal Getting

▪ Modelling, Calculation

- Software-Tool UMBERTO
- Weighted Index of Overall Effect

▪ Significant Conclusions

- Global Warming Potential Reduction by 67 %
- Improvement of Energy and Resource Efficiency by 33 % and 1 %

9. References

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- [10] <http://www.physicalgeography.net/fundamentals/7a.html>